Tuning of optimal P and PI controllers for level control of single tank system

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Abstract

In this paper, optimal P and PI controllers are proposed for level control of single tank system. The integral-square-error (ISE) of unit step response is considered as design criterion for obtaining optimal controller settings. This method of formulation of ISE requires only some alpha and beta parameters unlike integration with time. The teacher learner based optimization (TLBO) algorithm is employed for minimizing the performance index. It is found that the proposed TLBO based controllers provide excellent results in terms of time domain specifications.

Keywords

ISE, Level control, PID controller, Teacher learner based optimization, Tuning.

1.Introduction

Various methods have been proposed in the literature for obtaining optimal values of parameters of PID controller. Ziegler-Nichols (ZN) settings is one of the most used design criteria [1]. Other methods include integral of square time weighted error (ISTE), Pessen integral of absolute error (PIAE), Kessler Landau Voda (KLV), some overshoot rule (SO-OV), no overshoot rule (NO-OV), Mantz-Tacconi Ziegler-Nichols (MT-ZN) and refined Ziegler-Nichols (R-ZN) [2]. Other technique which provide better response in comparison to rule based tuning methods are PID controller tuning based on particle swarm Luus-Jaakola optimization [4]. optimization procedure for PID controller tuning [3], PID controller tuning based on genetic algorithm [6], evolutionary computation based PID tuning [5] and PID tuning using soft computing techniques [7].In this work, optimal P and PI controllers are proposed for level control of single tank system using teacher learner based optimization technique. The integralsquare-error (ISE) is considered as performance index. The ISE is obtained in terms of alpha and beta parameters. Being simple and efficient; the teacher learner based optimization (TLBO) is used minimizing the performance index [8-11]. The TLBO is easy to implement due to absence of algorithmspecific parameters.

The layout of this brief is as follows. Section 2 describes the system and its model. Section 3 provides the structure of controllers. The proposed method of tuning is discussed in section 4. The algorithm utilized to minimize the ISE is detailed in section 5. Section 6 provides results. The paper is concluded in section 7.

2.The single tank system

The block diagram shown in *Figure 1* illustrates the liquid level control of single tank system [12].

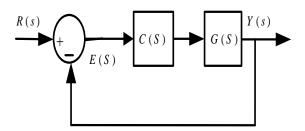


Figure 1 Single tank system

The transfer function of plant is given as

$$G(s) = \frac{K}{\left(\tau_a s + 1\right)} \tag{1}$$

where, *K* is gain and τ_a is time constant of tank. In block diagram, *C*(*s*) represents the controller transfer function.

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3.The controllers

The transfer function of PID controller is

$$C(s) = K_p \left(1 + \frac{1}{T_i s} + T_d s \right)$$
⁽²⁾

where, K_p , T_i and T_d are, respectively, the proportional gain, integral time constant and derivative time constant. The P and PI controller are given by (3)and (4), respectively.

$$C(s) = K_p \tag{3}$$

$$C(s) = K_p \left(1 + \frac{1}{T_i s} \right) \tag{4}$$

4.The TLBO based tuning method

In proposed work, the integral-square-error is considered as design criterion for tuning. The ISE is given as

$$J = \int_{t=0}^{t=\infty} e^2(t) dt \tag{5}$$

This can be written as

$$I = \frac{1}{2} \sum_{i=1}^{n} \frac{\beta_{i}^{2}}{\alpha_{i}}$$
(6)

in terms of alpha and beta parameters [13] where n is the order of error in *s*-domain. The alpha and beta parameters for error

$$E(s) = \frac{b_1 s^{n-1} + \dots + b_n}{a_0 s^n + a_1 s^{n-1} + \dots + a_n}$$
(7)

are given in *Table 1* and *Table 2*.

Table 1 Alpha table

	$c_0^0 = a_0$	$c_{2}^{0} = a_{2}$	$c_{4}^{0} = a_{4}$	$c_{6}^{0} = a_{6}$	•••
	$c_0^1 = a_1$	$c_{2}^{1} = a_{3}$	$c_{4}^{1} = a_{5}$	•••	
$\alpha_1 = c_0^0 / c_0^1$	$c_0^2 = c_2^0 - \alpha_1 c_2^1$	$c_2^2 = c_4^0 - \alpha_1 c_4^1$	$c_4^2 = c_6^0 - \alpha_1 c_6^1$	• • •	
$\alpha_2 = c_0^1 / c_0^2$	$c_0^3 = c_2^1 - \alpha_2 c_2^2$	$c_2^3 = c_4^1 - \alpha_2 c_4^2$	$c_4^3 = c_6^1 - \alpha_2 c_6^2$	•••	
$\alpha_3 = c_0^2 / c_0^3$	$c_0^4 = c_2^2 - \alpha_3 c_2^3$	$c_2^4 = c_4^2 - \alpha_3 c_4^3$:		
$lpha_{4}=c_{0}^{3}/c_{0}^{4}$	$c_0^5 = c_2^3 - \alpha_4 c_2^4$:			
$lpha_{5}=c_{0}^{4}/c_{0}^{5}$:				
:					

Table 2 Beta table

The error obtained in *s*-domain for system given in *Figure 1* can be written as

$$E(s) = R(s) - Y(s) = \frac{R(s)}{1 + G(s)C(s)}$$
(8)

where,

$$R(s) = \frac{1}{s} \tag{9}$$

5.Teacher learner based optimization (TLBO) algorithm

Recently, Rao et al. proposed TLBO algorithm [14]. This algorithm is composed of two phases namely teacher phase and learner phase. In former phase, the class teacher tries to improve the average performance of the class. In latter phase, learners compete among themselves and try to enhance their performance.

Suppose, the number of learners and subjects offered in the class are a total of R and C, respectively. The performance of *i*th learner, $i = 1, 2, \dots, R$, in *j*th subject, $j = 1, 2, \dots, C$ is given as $X_{i,j}$. In teacher phase, class performance is updated by:

$$newX_{i,j} = X_{i,j} + r\left(X_{\text{teacher},j} - T_f \ \bar{X}_{i,j}\right)$$
(10)

Where $newX_{i,j}$ is updated performance of the class and r is a random number in the range (0,1). $X_{\text{teacher},j}$ and $\overline{X}_{i,j}$ denote respectively the performance of class teacher (i.e. the best learner of the class) and mean performance of the class. The parameter T_f is called teacher factor which is given by

$$T_f = \{1, 2\} \tag{11}$$

At the end of teacher phase, $newX_{i,j}$ is updated if it denotes a better. In learner phase, learners' performance is updated

$$newX_{i,j} = X_{i,j} + r(X_{u,j} - X_{v,j})$$
(12)

Where *u* and *v* are randomly selected learners such that $u \neq v$, $f(X_{u,j}) < f(X_{v,j})$ and *r* is a random number such that r = (0,1). At the end of learner phase, the solution $newX_{i,j}$ is updated in *X* if it represents better solution. This completes teacher and learner phases of TLBO algorithm. These two phases are repeated until the termination criterion achieves.

The parameters [12] of single tank system are K = 5and $\tau_a = 2$.

P controller:

For the system given by(1), the error transfer function (7) becomes

$$E(s) = \frac{b_1 s + b_2}{a_0 s^2 + a_1 s + a_2}$$
(13)

where,

$$a_0 = \tau_a \tag{14}$$

$$a_1 = K K_p + 1 \tag{15}$$

$$a_2 = 0 \tag{16}$$

$$b_1 = \tau_a \tag{17}$$

$$b_2 = 1$$
 (18)

The alpha and beta tables (*Table 1* and *Table 2*) modifies to *Table 3* and *Table 4*, respectively.

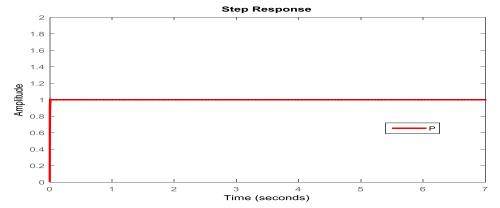
Table 3 Alpha table

$$\begin{array}{c|c} & c_0^0 = a_0 & c_2^0 = a_2 \\ c_0^1 = a_1 & c_2^1 = 0 \\ \hline \alpha_1 = c_0^0 / c_0^1 & c_0^2 = c_2^0 \\ \alpha_2 = c_0^1 / c_0^2 \end{array}$$

 Table 4 Beta table

$$\begin{array}{c|c} d_0^1 = b_1 & d_2^1 = 0 \\ d_0^2 = b_2 & d_2^2 = 0 \\ \hline \beta_1 = d_0^1 / c_0^1 & d_0^3 = 0 \\ \beta_2 = d_0^2 / c_0^2 & \end{array}$$

6.Results and discussion





The performance index, given by(6), becomes

$$J = \frac{1}{2} \sum_{i=1}^{2} \frac{\beta_i^2}{\alpha_i} = \frac{1}{2} \left\{ \frac{\beta_1^2}{\alpha_1} + \frac{\beta_2^2}{\alpha_2} \right\}$$
(19)

$$J = \frac{1}{2} \left\{ \frac{b_1^2}{a_0 a_1} + \frac{b_2^2}{a_1 a_2} \right\}$$
(20)

Minimizing (20) using TLBO, the optimal value of controller gain obtained is $K_p = 257.96$. Figure 2 provides the unit step response for the proposed setting. The settling time and peak over shoot are 0.006 seconds and 0% respectively.

PI controller:

whore

For (1), the error transfer function (7) turn out to be

$$E(s) = \frac{b_1 s + b_2}{a_0 s^2 + a_1 s + a_2}$$
(21)

$$a_0 = T_i \tau_a \tag{22}$$

 $a_1 = T_i \left(K K_p + 1 \right) \tag{23}$

$$a_2 = K K_n \tag{24}$$

$$b_1 = T_i \ \tau_a \tag{25}$$

$$b_2 = T_i \tag{26}$$

The alpha and beta tables (*Table 1* and *Table 2*) become, respectively, *Table 5* and *Table 6*.

Table 5 Alpha table

$$\begin{array}{c|c} & c_0^0 = a_0 & c_2^0 = a_2 \\ c_0^1 = a_1 & c_2^1 = 0 \\ \hline \hline \alpha_1 = c_0^0 \, / \, c_0^1 & c_0^2 = c_2^0 \\ \alpha_2 = c_0^1 \, / \, c_0^2 \end{array}$$

Table 6 Beta table

$$\begin{array}{c|c} d_0^1 = b_1 & d_2^1 = 0 \\ d_0^2 = b_2 & d_2^2 = 0 \\ \hline \beta_1 = d_0^1 / c_0^1 & d_0^3 = 0 \\ \beta_2 = d_0^2 / c_0^2 & \end{array}$$

The performance index, given by(6), modifies to

$$J = \frac{1}{2} \sum_{i=1}^{2} \frac{\beta_i^2}{\alpha_i} = \frac{1}{2} \left\{ \frac{\beta_1^2}{\alpha_1} + \frac{\beta_2^2}{\alpha_2} \right\}$$
(27)

$$J = \frac{1}{2} \left\{ \frac{b_1^2}{a_0 a_1} + \frac{b_2^2}{a_1 a_2} \right\}$$
(28)

Minimizing (28) using TLBO, the optimal values of controller gains obtained are $K_p = 100$ and $T_i = 8.03e - 12$. Figure 3 shows the step response obtained due to proposed settings. The settling time and peak over shoot obtained are 0.003 seconds and 99.40%, respectively.

From the proposed P and PI controllers, it is clear that the TLBO based tuning provides excellent results in terms of time domain specifications.

7.Conclusion

In this work, optimal P and PI controllers are proposed for level control of single tank system. The controller settings are obtained by minimizing the ISE of unit step response. This formulation of ISE requires a fixed number of alpha and beta parameters only. The teacher learner based optimization algorithm is employed for minimizing the performance index. The obtained controller settings provided excellent time response.

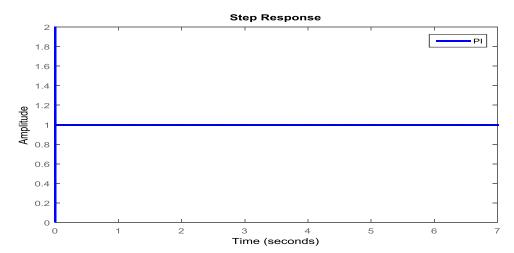


Figure 3 Step response of the system

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Acknowledgment

None.

Conflicts of interest

The authors have no conflicts of interest to declare.

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